AMENDMENTS TO THE CLAIMS:

This listing of claims will replace all prior versions, and listings, of claims in the application:

LISTING OF CLAIMS:

- (Currently Amended) A method for processing concentrates, 1. particularly concentrates produced from copper sulfide-based ores, characterized in that wherein the concentrate [(4)] to be processed, obtained from ore concentration, is divided into two sulfidic concentrates of different types, to a concentrate [[(7)]] mainly containing poorly soluble components such as the precious metals contained in the ore and containing sulfide-form iron, and to a concentrate [[(8)]] mainly containing well soluble components, and that the concentrate [[(8)]] containing soluble components is conducted to a leaching step [[(9)]], and the solution [[(13)]] obtained from said leaching step is conducted to at least one conversion step [[(11, 16)], and that in the conversion step [[(11)]] located first in the flowing direction, there is fed the concentrate [[(7)]] containing poorly soluble components, and that in the conversion step [[(11)]] that is located first in the flowing direction, at least the copper contained in the solution is converted to sulfidic form by means of the sulfideform iron of the concentrate [[(7)]] containing poorly soluble components, and that at least part of the solution [[(12)]] obtained from the conversion step [[(11, 16)]] is returned to the leaching step [[(9)]].
- 2. (Currently Amended) A method according to claim 1, characterized in that wherein in the conversion steps [[(16)]] following the conversion step that is

located first in the flowing direction, the different metal components are converted to sulfidic form by means of sulfide-form iron [[(17)]] fed into said conversion step.

- 3. (Currently Amended) A method according to claim 1 [[or 2]], characterized in that wherein the leaching [[(9)]] is carried out as atmospheric leaching at the temperature of 50-150°C.
- 4. (Currently Amended) A method according to claim 1 [[or 2]], characterized in that wherein the leaching [[(9)]] is carried out as autoclave leaching.
- 5. (Currently Amended) A method according to any of the preceding claims, characterized in that claim 1, wherein the conversion step [[(11, 16)]] is carried out at the temperature of 90-200°C.
- 6. (Currently Amended) A method according to claim 5, characterized in that wherein the conversion step [[(11, 16)]] is carried out at the temperature of 150-190°C.
- 7. (Currently Amended) A method according to any of the preceding claims, characterized in that claim 1, wherein the iron added in the first conversion step [[(11)]] in the flowing direction is chalcopyrite (CuFeS₂).

- 8. (Currently Amended) A method according to any of the preceding claims, characterized in that claim 1, wherein the iron added in [[the]] a conversion step [[(16)]] that is next in succession after the first conversion step is troilite (FeS).
- 9. (Currently Amended) A method according to any of the preceding claims 1-6, characterized in that claim 1, wherein the iron added in [[the]] a conversion step [[(16)]] that is next in succession after the first conversion step is pyrrhotite (Fe_{1-x}S).
- 10. (Currently Amended) A method according to <u>claim 1</u>, <u>any of the</u>

 preceding claims, characterized in that the <u>wherein a</u> flotation process [[(19)]] <u>is</u> used for producing the concentrates <u>and</u> is controlled by means of mineral-specific electrochemical measurements.
- 11. (Currently Amended) A method according to any of the preceding claims, characterized in that claim 1, wherein the leaching step [[(9)]] used in the treatment of the concentrate is controlled by means of mineral-specific electrochemical measurements.
- 12. (Currently Amended) A method according to any of the preceding claims, characterized in that claim 1, wherein the conversion step [[(11, 16)]] used in the treatment of the concentrate is controlled by means of mineral-specific electrochemical measurements.

13. (Currently Amended) A method according to any of the preceding claims, characterized in that claim 1, wherein in the conversion step [[(11)]] that is located first in the flowing direction, the precious metals contained in the concentrates are recovered.